



# Covalently anchoring covalent organic framework on carbon nanotubes for highly efficient electrocatalytic CO<sub>2</sub> reduction

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## ABSTRACT

Porphyrin-based covalent organic frameworks (Por-COF) nanosheets were vertically anchored on carbon nanotubes (CNT) with covalent connection for efficient electrocatalytic CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR). The CNT not only acts as ideal carriers for the dispersion of Por-COF but also facilitates electron transfer along porphyrin planes to immobilized metal active sites. As a result, covalently linked MWCNT-Por-COF-M (M: Co, Ni, Fe) display improved electrocatalytic CO<sub>2</sub>-to-CO activity and selectivity compared to pure Por-COF-M and MWCNT@Por-COF-M without covalent connection between two components. In particular, MWCNT-Por-COF-Co exhibits superior activity (FE<sub>CO</sub>: 99.3%), higher partial current density and good durability in 0.5 M KHCO<sub>3</sub> by H-type cell, while MWCNT-Por-COF-Cu exhibits the highest CH<sub>4</sub> faradaic efficiency of 71.2% in 1.0 M KOH by flow cell. The results of HRTEM and Auger spectrum revealed that the high performance of MWCNT-Por-COF-Cu could be attributed to the generated Copper-based nanoclusters during the electrocatalytic CO<sub>2</sub>RR process.

## 1. Introduction

Global energy demands and environment issues support broad research interest in CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR) for its ideal way to realize recycling utilization of carbon resources [1–6]. Within this context, electrocatalytic CO<sub>2</sub>RR offers a potential approach for sustainable and efficient conversion of CO<sub>2</sub> to value-added carbon products [7–16]. However, owing to the inherent thermodynamic stability of C=O chemical bond in CO<sub>2</sub> (750 kJ mol<sup>-1</sup>) [17], electrocatalytic CO<sub>2</sub>RR generally needs to overcome a high activation barrier. Moreover, the competitive reaction of hydrogen evolution reaction (HER) and the similar redox potentials of various CO<sub>2</sub>RR products usually result in poor selectivity and low conversion efficiency, which limit their practical application [18,19]. To solve these issues, researchers have explored different types of electrocatalytic CO<sub>2</sub>RR materials, such as metals [20, 21], metal dichalcogenide [22], transition metal oxide [23,24] and metal-free 2D materials (g-C<sub>3</sub>N<sub>4</sub>) [25]. In spite of the tremendous efforts and glorious achievements, the studies in this field still have some challenges, such as weak CO<sub>2</sub> adsorption and activation capacity of

catalysts, slow reaction kinetics, low electron transmission efficiency and poor product selectivity [26,27].

Covalent-organic frameworks (COFs), as a new class of crystalline and porous material has recently attracted enormous attention for their variety of applications including gas storage [28,29], chemical sensing [30], drug delivery [31,32] and catalysis [33] due to their well-defined structure, high stability and inherent porosity [34,35]. In the past few years, COFs have appeared as a new kind of electrocatalytic CO<sub>2</sub>RR materials by incorporating metal ions as active sites. Especially, the excellent electrocatalytic CO<sub>2</sub>RR activities of some porphyrin-based COFs, such as COF-366, COF-367, TTCOF, have been confirmed in pioneer works for the electronic character of porphyrin active sites and high charge carrier mobility along porphyrin plane [36–42]. Although this encouraging progress, the inefficient electrical conduction between layers generally results in low electron transmission efficiency in most of bulk COFs materials, which limits further enhancing their electrocatalytic CO<sub>2</sub>RR activity. Thus, rationally integrating COFs with conductive support to construct COF-based composite materials with effective electron transfer capability holds interesting prospects for

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highly efficient electrocatalytic CO<sub>2</sub>RR. However, this strategy of combining COFs and conductive support for electrocatalytic CO<sub>2</sub>RR has not been systematically explored.

As one of the most famous conductive material, carbon nanotubes (CNT) are a promising candidate for supporting various catalysts due to their intrinsic physical properties including superior mechanical strength and electrical conductivity [43–45], which can provide consecutive tunneling for electron transfers. Multiple molecular catalysts (such as metalloprophyrin and metallophthalocyanine etc.) have been immobilized on CNT by  $\pi$ - $\pi$  interaction for efficient electrocatalytic CO<sub>2</sub> conversion [46–48]. Differently from the immobilized molecular catalysts on CNT, 2D COFs are assembled with conjugated multilayer. We reasoned, the combination of CNT and COFs by  $\pi$ - $\pi$  interaction may lead to relatively high resistance of electron transfer by accrossing COFs interlayer, while controlling the combination mode of CNT and COFs to realize electron conduction along porphyrin-based plane of COFs should be beneficial for the transfer of electrons to metal active sites. Moreover, a strong bonded connection of COFs and CNT that can facilitate electron transfer from CNT to COFs layers is also essential for high electrocatalytic performance of the resultant material as well as the solid integration of them.

Based on the above consideration, we integrate Por-COF with CNT by covalent bonds constructing a series of covalently connected MWCNT-Por-COF-M for efficient electrocatalytic CO<sub>2</sub>RR. To realize the formation of covalent bonds between CNT and Por-COF and effective electron transmission along porphyrin-based plane of Por-COF, -NH<sub>2</sub> group modified MWCNT was chosen to bond Pro-COF and disperse Pro-COF nanosheets by in-situ reaction. As a result, ultra-small Por-COF nanosheets were covalently anchored on the surface of MWCNT with uniform dispersion (Scheme 1). After chelating different metal ions, a series of MWCNT-Por-COF-M show higher electrocatalytic CO<sub>2</sub>-to-CO activity and selectivity compared to pure Por-COF-M. In particular, the MWCNT-Por-COF-Co shows the highest CO Faraday efficiency up to 99.3% at the potential of  $-0.6$  V and a current density of  $18.77 \text{ mA cm}^{-2}$  at  $-1.0$  V.

Further experiments clarified that the superior electrocatalytic activity of MWCNT-Por-COF-Co is mainly attributed to more efficient electron transfer during the CO<sub>2</sub>RR reaction process. Furthermore, we also investigated the electrocatalytic CO<sub>2</sub> reduction activity of MWCNT-Por-COF-Cu in 1.0 M KOH by flow cell. The results show that MWCNT-Por-COF-Cu exhibits the highest CH<sub>4</sub> faradaic efficiency of 71.2%. The results of HRTEM and Auger spectrum revealed that the high performance of MWCNT-Por-COF-Cu could be attributed to the generated Copper-based nanoclusters during the electrocatalytic CO<sub>2</sub>RR process.

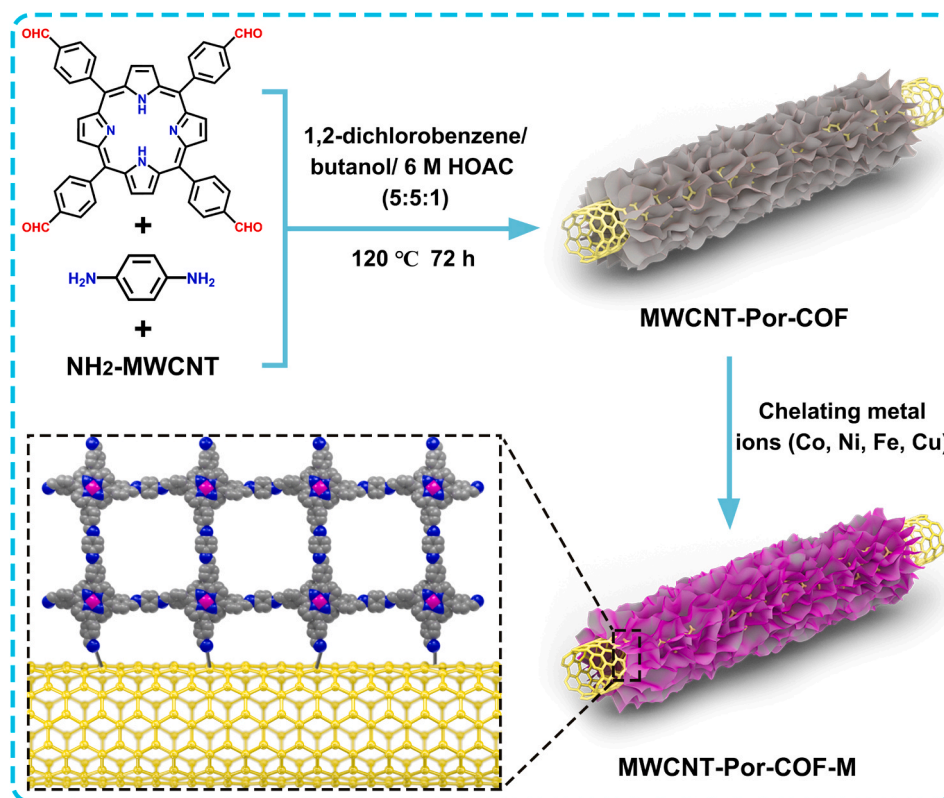
## 2. Experimental section

### 2.1. Materials

All of the reagents and solvents were commercially available and used without further purification. Por-CHO ( $\geq 98\%$ ) was purchased from Jilin Chinese Academy of Sciences-Yanshen Technology Co., Ltd.

### 2.2. Instrumentation

Infrared spectrum using the KBr pellet was measured on a Bruker Tensor 27 in the range of  $4000\text{--}400 \text{ cm}^{-1}$ . Scanning electron microscopy (SEM) micrographs were recorded on a Hitachi S-4800 instrument operating at 20 kV. Transmission electron microscope (TEM) images were taken on a JEM-2100 microscope equipped. X-ray powder diffraction (PXRD) patterns were recorded on a DX-2700B X-ray diffractometer. The patterns were collected at a scanning rate of  $5^\circ$  per min in the  $2\theta$  range from  $5^\circ$  to  $50^\circ$ . Nitrogen adsorption-desorption isotherms were measured at 77 K on a Micromeritics ASAP 2020 adsorptometer, and CO<sub>2</sub> adsorption isotherms were measured at 298 K. X-ray photoelectron spectroscopy (XPS) study was performed on the Kratos Axis Ultra DLD.



**Scheme 1.** Schematic diagram of synthetic process of the MWCNT-Por-COF-M (M: Co, Ni, Fe, Cu) composite materials.

### 2.3. Synthesis of Por-COF

According to previous reported procedures [38]. A vacuum valve measuring o.d*×*i.d. = 19 × 8 mm<sup>2</sup> and length 65 mm was charged with Por-CHO (72.6 mg, 0.10 mmol), *p*-phenylenediamine (21.6 mg, 0.20 mmol), 2.5 mL butanol, 2.5 mL 1,2-dichlorobenzene, and 0.5 mL of 6 mol/L aqueous acetic acid. This solution was then sonicated for 20 min to form a homogeneous dispersion. Afterwards, the vacuum valve was flash frozen in a liquid N<sub>2</sub> bath (77 K) and degassed by three freeze-pump-thaw cycles, sealed under vacuum, and then heated at 120 °C for 3 days. The products were collected by centrifugation or filtration and washed with anhydrous THF (50 mL) for three times. The powders collected were soaked in anhydrous acetone for 48 h, replaced the solvent for 5–6 times and then dried at 180 °C for 12 h under vacuum to afford Por-COF materials.

### 2.4. Synthesis of MWCNT-Por-COF

A vacuum valve measuring o.d*×*i.d. = 19 × 8 mm<sup>2</sup> and length 65 mm was charged with Por-CHO (40 mg), different quality of NH<sub>2</sub>-MWCNT (30, 50, 70, 90, 120 mg), 2.5 mL butanol, and 2.5 mL 1,2-dichlorobenzene. This solution was then sonicated for 20 min to form a homogeneous dispersion solution. Then *p*-phenylenediamine (10.08 mg, 0.10 mmol) was added in above homogeneous solution and continue sonicated for 20 min. Finally, 0.5 mL of 6 mol/L aqueous acetic acid was added in above homogeneous solution. Afterwards, the vacuum valve was flash frozen in a liquid N<sub>2</sub> bath (77 K) and degassed by three freeze-pump-thaw cycles, sealed under vacuum, and then heated at 120 °C for 3 days. The products were collected by centrifugation or filtration and washed with anhydrous THF (50 mL) for three times. The powders collected were soaked in anhydrous acetone for 48 h, replaced the solvent for 5–6 times and then dried at 180 °C for 12 h under vacuum to afford different weight ratios of NH<sub>2</sub>-MWCNT(X)-Por-COF composite materials.

### 2.5. Synthesis of various MWCNT-Por-COF-M

CoCl<sub>2</sub>·6 H<sub>2</sub>O (100 mg) (or FeCl<sub>2</sub>·4 H<sub>2</sub>O, NiCl<sub>2</sub>·6 H<sub>2</sub>O, CuCl<sub>2</sub>·6 H<sub>2</sub>O), MWCNT-Por-COF (50 mg), and Tetrahydrofuran (THF) (40 mL) were mixed and heated at 50 °C for 15 h. The powder was collected by filtration and washed with THF and acetone for several times. Finally, the powder was dried in vacuum at 120 °C for 48 h. For NiCl<sub>2</sub>·6 H<sub>2</sub>O, the THF was replaced with acetonitrile (CH<sub>3</sub>CN), because NiCl<sub>2</sub>·6 H<sub>2</sub>O is insoluble in THF.

### 2.6. Synthesis of amino-free functionalized MWCNT@Por-COF-Co

MWCNT@Por-COF-Co composite material was prepared by the above method except that was amino-free functionalized MWCNT replaced by NH<sub>2</sub>-MWCNT.

### 2.7. Electrochemical measurements of H-type cell

The H-type cell tests of the catalysts were performed at ambient environment on the electrochemical workstation (CHI660E) in a standard three-electrode configuration in 0.5 M KHCO<sub>3</sub>. Carbon rod and Ag/AgCl electrode were used as the counter and reference electrode, respectively. The experiment was performed in an airtight electrochemical H-type cell with a catalyst-modified carbon cloth electrode (CCE, 1 cm × 2 cm) as the work electrode. Nafion solution was introduced as a kind of electrocatalyst dispersion solution, which can form a homogeneous ink with MWCNT-Por-COF-M and further help to attach onto the surface of carbon cloth. The preparation procedures of the CCE working electrode were presented as follows: 10 mg electrocatalyst, and 1 mL 0.5% Nafion solution were grounded to form uniform catalyst ink. After sonication for 30 min, the ink was dropped directly onto a carbon

cloth (1 cm × 1 cm) with a catalyst loading density of ~1 mg cm<sup>-2</sup> and dried. In the H-type cell, two compartments were separated by an exchange membrane (Nafion®117). During the electrocatalytic CO<sub>2</sub>RR experiments, the polarization curves were performed by LSV mode at a scan rate of 2 mV s<sup>-1</sup>. Initially, polarization curves for the modified electrode were recorded under an inert N<sub>2</sub> atmosphere. After that, the solution was bubbled with CO<sub>2</sub> (99.999%) for at least 30 min to make the aqueous solution saturated and then the electrocatalytic CO<sub>2</sub>RR test was conducted. Potential was measured vs. Ag/AgCl electrode and the results were reported vs. RHE based on the Nernst equation: E (vs. RHE) = E (vs. Ag/AgCl) + 0.1989 V + 0.059 × pH. EIS spectroscopy measurement was carried out by applying an AC voltage with 10 mV amplitude in a frequency range from 1000 kHz to 100 mHz at overpotential of -0.7 V (vs. RHE). To estimate the ECSA, CV were tested by measuring Cdl under the potential window range from 0 V to 0.1 V (vs. RHE) with various scan rates from 10 to 100 mV s<sup>-1</sup>. All the LSV curves were presented without iR compensation.

### 2.8. Electrochemical measurements of flow cell

CO<sub>2</sub> electrolysis was performed in a three-channel flow cell composed of a gas-diffusion layer (GDL), an anion exchange membrane (Fumasep, FAA-3-PK-130) and a Pt plate (1 cm<sup>2</sup>) anode as shown in Scheme S1. The prepared catalyst and gas-diffusion layer, anion exchange membrane and Pt anode were clamped together in order using polytetrafluoroethylene (PTFE) spacers and then fixed with screws. The electrolyte (1.0 M KOH aqueous solution) was then introduced into the chamber between membrane and the cathode as well as the chamber between the anode and membrane. The electrolyte in cathode and anode were circulated by a peristaltic pump (LongerPump, BT100-2 J), with the flow rate of 5 mL min<sup>-1</sup>. The high-purity CO<sub>2</sub> (99.999%) gas was continuously passed through the flow chamber which is behind the gas-diffusion layer and diffuse into the electrolyte present at the catalyst. The gas flow rate was set as 20 sccm via a mass flow controller (AITOLY, MFC300). A saturated Ag/AgCl reference electrode (CHI111) was located in the catholyte stream and positioned ≈ 1 cm from the cathode was used to measure the cathodic half-cell potential.

### 2.9. Reaction product analysis and calculation

The electrolysis was carried out in an airtight electrochemical H-type cell at selected potentials (-0.5 to -1.0 V) to determine the reduction products and their Faradic efficiency. The gaseous reduction products (e.g., CO) were monitored by a GC (GC-7920) equipped with a flame ionization detector. During the test, nitrogen was the carrier gas. A TCD was used to analyze hydrogen with nitrogen as the carrier gas. The liquid products were collected from the cathode chambers after electrolysis and detected by IC spectroscopy.

The calculation of Faradaic efficiency.

For CO,

$$FE = \frac{2n_{\text{CO}} \times F}{Q} \times 100\% \quad (1)$$

For H<sub>2</sub>,

$$FE = \frac{2n_{\text{H}_2} \times F}{Q} \times 100\% \quad (2)$$

where F is the Faraday constant (F = 96485 C/mol), n<sub>CO</sub> is the moles of produced CO, Q is the total charge (C), and n<sub>H<sub>2</sub></sub> is the moles of produced H<sub>2</sub>.

The faradaic efficiencies for flow cell were calculated using the following equation:

$$FE = \frac{nFxV}{j_{\text{Tot}}} \quad (3)$$



Where  $n$  = number of electrons transferred.

$F$  = Faraday's constant.

$x$  = mole fraction of product.

$V$  = total molar flow rate of gas.

$j_{\text{Tot}}$  = total current.

Turnover frequency (TOF,  $\text{s}^{-1}$ ).

The TOF for CO was calculated as follows:

$$\text{TOF} = \frac{i \times FE_{\text{CO}}}{2F \times n_{\text{cat}}} \quad (4)$$

where  $i$  is the current,  $n_{\text{cat}}$  is the total moles of catalyst employed in the electrolysis.

The calculation of energy efficiency (EE)

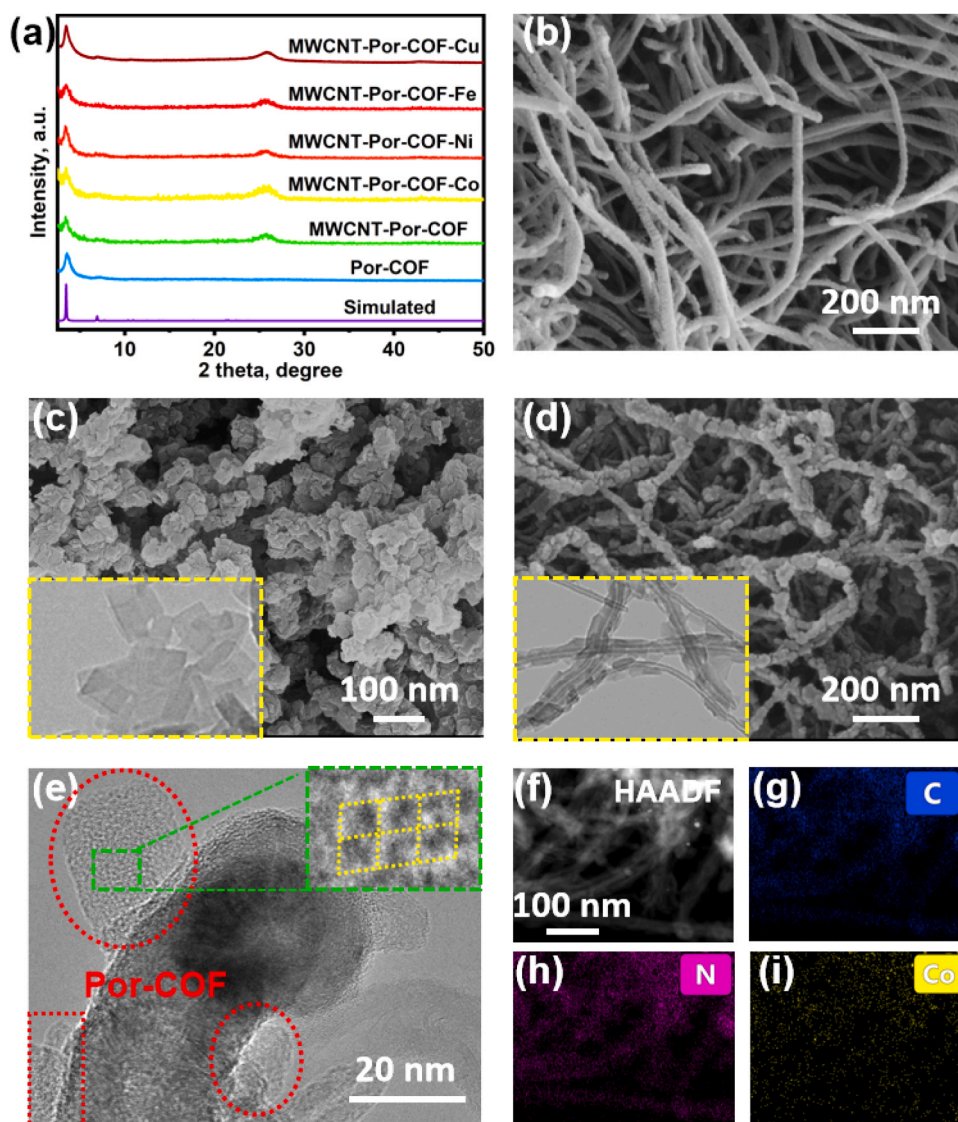
$$EE = \frac{E_{\text{CO}} \times FE_{\text{CO}}}{E_{\text{CO}} + \eta} \times 100\% \quad (5)$$

where  $E_{\text{CO}}$  (V) is the equilibrium cell potential for CO,  $FE_{\text{CO}}$  (%) is the Faradaic efficiency of CO,  $\eta$  (V) is the overpotential.

### 3. Results and discussion

#### 3.1. Preparation process and structure characterization

Por-COF was synthesized by condensing 5,10,15,20-Tetrakis(4-benzaldehyde)porphyrin (Por-CHO) and *p*-phenylenediamine in a mixture of butanol/1,2-dichlorobenzene/AcOH (5:5:1) under solvothermal conditions [49]. Fourier-transform infrared (FT-IR) spectrum of Por-COF shows a new peak at  $1617 \text{ cm}^{-1}$  attributed to the formation of C=N bond (Fig. S1), along with the dismissing of characteristic bands of -CHO ( $1700 \text{ cm}^{-1}$ ) group in Por-CHO and  $\text{-NH}_2$  ( $3369 \text{ cm}^{-1}$ ) in *p*-phenylenediamine. In addition, the powder X-ray diffraction (PXRD) pattern of Por-COF matches well with the simulated PXRD pattern indicating successful synthesis of Por-COF (Fig. S2). A series of covalently connected MWCNT(X)-Por-COF ( $X = 50, 62, 70, 75, 80 \text{ wt\%}$ ) composites with different contents of MWCNT were synthesized by adding variably quantitative  $\text{NH}_2$ -MWCNT into the above reaction system of Por-COF. The PXRD patterns of MWCNT(X)-Por-COF support the successful synthesis of these composites for the appearance of a new peak at 28 degrees from MWCNT (Fig. S2). The resultant MWCNT-Por-COF-M ( $X = 70 \text{ wt\%}$ , M: Co, Ni, Fe) composites were obtained by coordinating different transition metal ions ( $\text{Co}^{2+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Fe}^{2+}$ )



**Fig. 1.** (a) PXRD patterns of MWCNT-Por-COF-M (M: Co, Ni, Fe, Cu). (b-d) SEM and TEM (inset) images of  $\text{NH}_2$ -MWCNT, Por-COF and MWCNT-Por-COF. (e) HRTEM image and pores (inset) of MWCNT-Por-COF. (f-i) HAADF and elements mapping images of MWCNT-Por-COF-Co.

onto porphyrin moiety of these materials. As presented in Fig. 1a, the PXRD patterns of MWCNT-Por-COF-M (Co, Ni, Fe, Cu) agree well with the parent Por-COF, and the main peaks in FT-IR spectra of MWCNT-Por-COF-M also do not change apparently (Fig. S3). XPS measurements of MWCNT-Por-COF-M (M: Co, Ni, Fe) confirm that the metal centers in MWCNT-Por-COF-M are all bivalence (Fig. S4-S6). The Cu 2p XPS clearly demonstrated that MWCNT-Por-COF-Cu displays two peaks at the binding energy of 935.0 and 954.8 eV attributed to Cu 2p<sub>3/2</sub> and Cu 2p<sub>1/2</sub> of Cu<sup>2+</sup> species from the coordinated Cu center in Por-COF-Cu, and no the Cu<sup>+</sup> and Cu<sup>0</sup> state were observed in XPS (Fig. S7).

In order to verify the formation of covalent bonds between NH<sub>2</sub>-MWCNT and Por-COF, two model compounds were prepared by solvothermal reaction and mechanical grinding of Por-CHO and NH<sub>2</sub>-MWCNT, named as Por-CHO-MWCNT-Reaction and Por-CHO-MWCNT-Grinding, respectively. The FT-IR results show a new peak at 1655 cm<sup>-1</sup> from stretching vibration peak of C=N appeared for Por-CHO-MWCNT-Reaction and Por-CHO-MWCNT-Grinding in comparison with NH<sub>2</sub>-MWCNT (Fig. S8). Compared to Por-CHO-MWCNT-Grinding, the relative intensity of C=N stretching vibration peak of Por-CHO-MWCNT-Reaction is higher demonstrating that solvothermal reaction is more prone to the formation C=N by Schiff-base reaction of Por-CHO and NH<sub>2</sub>-MWCNT. In the XPS spectra, the peak of N 1s in C=N of Por-CHO-MWCNT-Reaction is significantly higher than that of Por-CHO-MWCNT-Grinding and NH<sub>2</sub>-MWCNT (Fig. S9), indicating the formation of new C=N bonds by the reaction of Por-CHO and NH<sub>2</sub>-MWCNT in this reaction condition. The formation of C=N bonds in Por-CHO-MWCNT-Reaction supports the covalent connection of NH<sub>2</sub>-MWCNT and Por-COF in MWCNT-Por-COF.

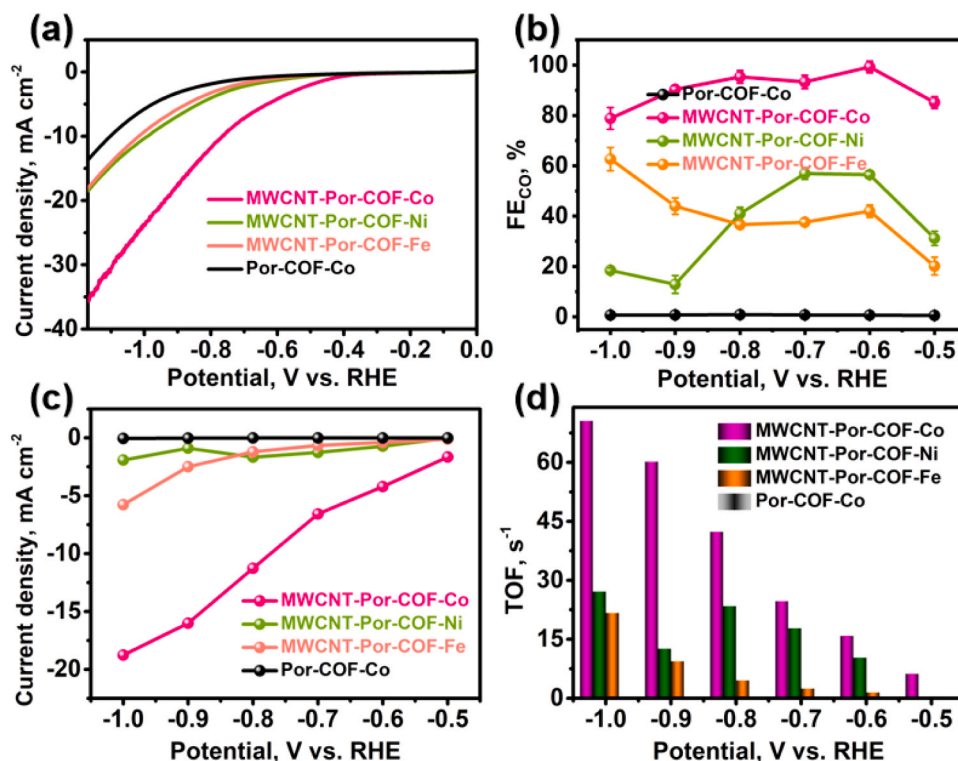
### 3.2. Morphology and porosity structural characterization

The morphology of MWCNT-Por-COF-M was characterized by scanning electron microscopy (SEM) and transmission electron microscopy (TEM). The NH<sub>2</sub>-MWCNT presents typical nanotube morphology with a smooth surface (Fig. 1b). The pure Por-COF shows sheet-like nanocrystals around 30 nm which were seriously aggregated together (Fig. 1c). As presented in Fig. 1d, the nanocrystals of Por-COF were uniformly anchored on the surface of CNT in MWCNT-Por-COF. The results of TEM measurement for MWCNT-Por-COF further confirm Por-COF was grown surround CNT with uniform dispersion by the in-situ reaction (Fig. 1e). Moreover, the porous Por-COF nanosheets were anchored on MWCNT with the edge of (100) plane (Fig. 1e inset). For comparison, we also synthesized non-covalently connected MWCNT@Por-COF with MWCNT (without modified -NH<sub>2</sub> groups) as precursor. The SEM image of MWCNT@Por-COF shows Por-COF and MWCNT mainly exist separately (Fig. S10). These results demonstrate the essential role of modified -NH<sub>2</sub> groups on NH<sub>2</sub>-MWCNT for the dispersion of Por-COF on MWCNT and avoiding the aggregation of Por-COF in the resultant composites. After the coordination of metal ions, the morphology of the series of MWCNT-Por-COF-M have no apparent change as confirmed by SEM (Fig. S11). SEM and TEM images of MWCNT-Por-COF-Cu show the same morphology as the above MWCNT-Por-COF-M (Co, Ni, Fe) (Fig. S12). Furthermore, the elemental mapping and energy dispersive spectroscopy (EDS) for MWCNT-Por-COF-Co were detected. The results show that N and Co elements were uniformly distributed on the CNT (Figs. 1f-1i), and the content of Co element was 1.9 wt% in the EDS, which was lower than theoretical value (6.3 wt%) (Fig. S13). The porosity structural of Por-COF and MWCNT-Por-COF-M were investigated by N<sub>2</sub> absorption and desorption curves at 77 K. The results indicate that all the samples exhibit type I absorption isotherms (Fig. S14-S15) and the pore size distributions are concentrated on 15 Å, similar to that reported previously (Fig. S16) [38].

### 3.3. Electrocatalytic CO<sub>2</sub>RR performances in H-type cell

The electrocatalytic CO<sub>2</sub>RR performances for MWCNT-Por-COF-M (M: Co, Ni, Fe) were evaluated in gas-tight H-type electrochemical cell (separated by a Nafion®117 proton exchange membrane) with CO<sub>2</sub>-saturated 0.5 M KHCO<sub>3</sub> as electrolyte. Before measurements, MWCNT-Por-COF-M were immersed in 0.5 M KHCO<sub>3</sub> aqueous solution for 50 h, the identical PXRD patterns before and after immersed demonstrate their structural stability at this condition (Fig. S17). The results of Faradic efficiency for MWCNT-Por-COF-Co support that the different content of NH<sub>2</sub>-MWCNT as precursor is the optimism ratio for the electrocatalytic activity of the resultant composites (Fig. S18). For different MWCNT-Por-COF-M, Linear sweep voltammetry (LSV) curves show that MWCNT-Por-COF-Co possesses the smallest onset potential and large current density in CO<sub>2</sub>-saturated KHCO<sub>3</sub> than that of MWCNT-Por-COF-Ni and MWCNT-Por-COF-Fe (Fig. 2a), demonstrating its much higher CO<sub>2</sub>RR activity. In addition, compared to the condition of Ar-saturated KHCO<sub>3</sub> solution, the MWCNT-Por-COF-Co shows a much higher current density and smaller onset potential in CO<sub>2</sub>-saturated KHCO<sub>3</sub> solution (Fig. S19), indicating higher CO<sub>2</sub>RR reaction activity than HER [50,51]. To evaluate the selectivity of MWCNT-Por-COF-M for CO<sub>2</sub>RR, the reduction products were analyzed by gas chromatography (GC) and Ion chromatography. The results show that CO is the primary reduction product accompanied by a small amount of H<sub>2</sub> from reduced water and there is no detected liquid product by Ion chromatography (Fig. S20-S21). Subsequently, the corresponding Faradic efficiency of CO and H<sub>2</sub> are calculated at -0.5 to -1.0 V to further evaluate the electrocatalytic CO<sub>2</sub>RR selectivity of the MWCNT-Por-COF-M. As shown in Fig. 2b and S22, the MWCNT-Por-COF-Co showed the best electrocatalytic activity for CO<sub>2</sub>-to-CO conversion with the highest CO Faradaic efficiency (FE<sub>CO</sub>) of 99.3% at -0.6 V, which was obviously higher than that of MWCNT-Por-COF-Fe (42.1%), MWCNT-Por-COF-Ni (56.4%) and individual Por-COF-Co (1.6%) at the same potential. Furthermore, the MWCNT-Por-COF-Co also maintains excellent FE<sub>CO</sub> (> 90%) at -0.6 to -0.9 V, which outperforms many reported COF-based materials (Table S1) [36-38,40,52-54]. Moreover, the energy efficiency (EE) of MWCNT-Por-COF-Co was calculated to evaluate the energy conversion efficiency in CO<sub>2</sub>RR process. The result shows MWCNT-Por-COF-Co displays the largest EE of 87.62% at -0.6 V attributed to lower overpotential in the CO<sub>2</sub>RR process (Fig. S23).

To confirm the contribution of covalent connection between MWCNT and Por-COF to the improved electrocatalytic activity of MWCNT-Por-COF-Co, the electrocatalytic CO<sub>2</sub>RR activities of MWCNT@Por-COF-Co without covalent bonds connection and physical mixing sample of NH<sub>2</sub>-MWCNT and Por-COF-Co were determined (Fig. S24-S25). The results show covalently connected MWCNT-Por-COF-Co exhibits apparently higher FE<sub>CO</sub> (99.3%) for CO<sub>2</sub>-to-CO conversion than that of non-covalently connected MWCNT@Por-COF-Co (76.8%) and NH<sub>2</sub>-MWCNT/Por-COF-Co (46.3%). Thus, the excellent electrocatalytic CO<sub>2</sub>RR activity of MWCNT-Por-COF-Co should be attributed to the contribution of covalent connection between CNT and Por-COF which not only ensure the uniform distribution of Por-COF on CNT, but also enables the fluent transfer of electrons from CNT to metal active sites along covalently connected porphyrin planes. The partial current density of CO was carried out to deeply understand the efficiency of MWCNT-Por-COF-M for electrocatalytic CO<sub>2</sub>RR. As shown in Fig. 2c, the MWCNT-Por-COF-Co displays a current density of -18.77 mA cm<sup>-2</sup> at -1.0 V, which is much higher than that of MWCNT-Por-COF-Ni (-1.95 mA cm<sup>-2</sup>), MWCNT-Por-COF-Fe (-5.77 mA cm<sup>-2</sup>) and individual Por-COF-Co (0.05 mA cm<sup>-2</sup>). In addition, the turnover frequency (TOF) of MWCNT-Por-COF-Co was calculated to be 70.6 s<sup>-1</sup> at -1.0 V, which is also superior to MWCNT-Por-COF-Ni, MWCNT-Por-COF-Fe and individual Por-COF-Co (Fig. 2d). Besides, the <sup>13</sup>C-isotopic tracer experiment was carried out to reveal the carbon source of CO under the same reaction conditions. The products were analyzed by gas chromatography-mass spectrometry (GC-MS). The



**Fig. 2.** (a) LSV curves, (b) The FE of CO calculated potential ranges from  $-0.5$  to  $-1.0$  V, (c) The partial current density of CO, and (d) TOFs at different potentials for Por-COF and MWCNT-Por-COF-M (M: Co, Ni, Fe).

result shows the peak at  $m/z = 29$  is distributed to  $^{13}\text{CO}$ , revealed that the carbon source of CO come from  $\text{CO}_2$  molecules in the electrocatalytic process (Fig. 3a).

To elucidate the reaction kinetics activity of MWCNT-Por-COF-M for electrochemical  $\text{CO}_2\text{RR}$ , Tafel slopes were calculated. As presented in Fig. 3b, the Tafel slope of MWCNT-Por-COF-Co is calculated to be  $319 \text{ mV dec}^{-1}$ , which is much smaller than that of MWCNT-Por-COF-Ni ( $468 \text{ mV dec}^{-1}$ ) and MWCNT-Por-COF-Fe ( $541 \text{ mV dec}^{-1}$ ). The result indicates the favorable kinetics of MWCNT-Por-COF-Co for the  $\text{CO}_2$ -to-CO conversion attributed to more efficient charge transfer during  $\text{CO}_2\text{RR}$  process. Moreover, electrochemical double-layer capacitance ( $C_{dl}$ ) was calculated by measuring cyclic voltammetry (CV) curves in the non-faradaic region with different scan rates ( $10\text{--}100 \text{ mV s}^{-1}$ ) to evaluate the electrochemical active surface area (ECSA) (Fig. S26–S28). As presented in Fig. 3c, MWCNT-Por-COF-Co exhibits the largest  $C_{dl}$  of  $21.8 \text{ mF cm}^{-2}$  than MWCNT-Por-COF-Ni ( $15.7 \text{ mF cm}^{-2}$ ) and MWCNT-Por-COF-Fe ( $17.6 \text{ mF cm}^{-2}$ ), indicating that MWCNT-Por-COF-Co has a larger electrochemical area, which might provide more efficient active sites for electrocatalytic  $\text{CO}_2\text{RR}$ . Furthermore, covalently connected MWCNT-Por-COF-Co exhibits the larger  $C_{dl}$  than MWCNT@Por-COF-Co ( $14.8 \text{ mF cm}^{-2}$ ) without covalent bonds connection (Fig. S29–S30), indicating more metal centers of MWCNT-Por-COF-Co can be excited in during electrocatalytic  $\text{CO}_2\text{RR}$  process.

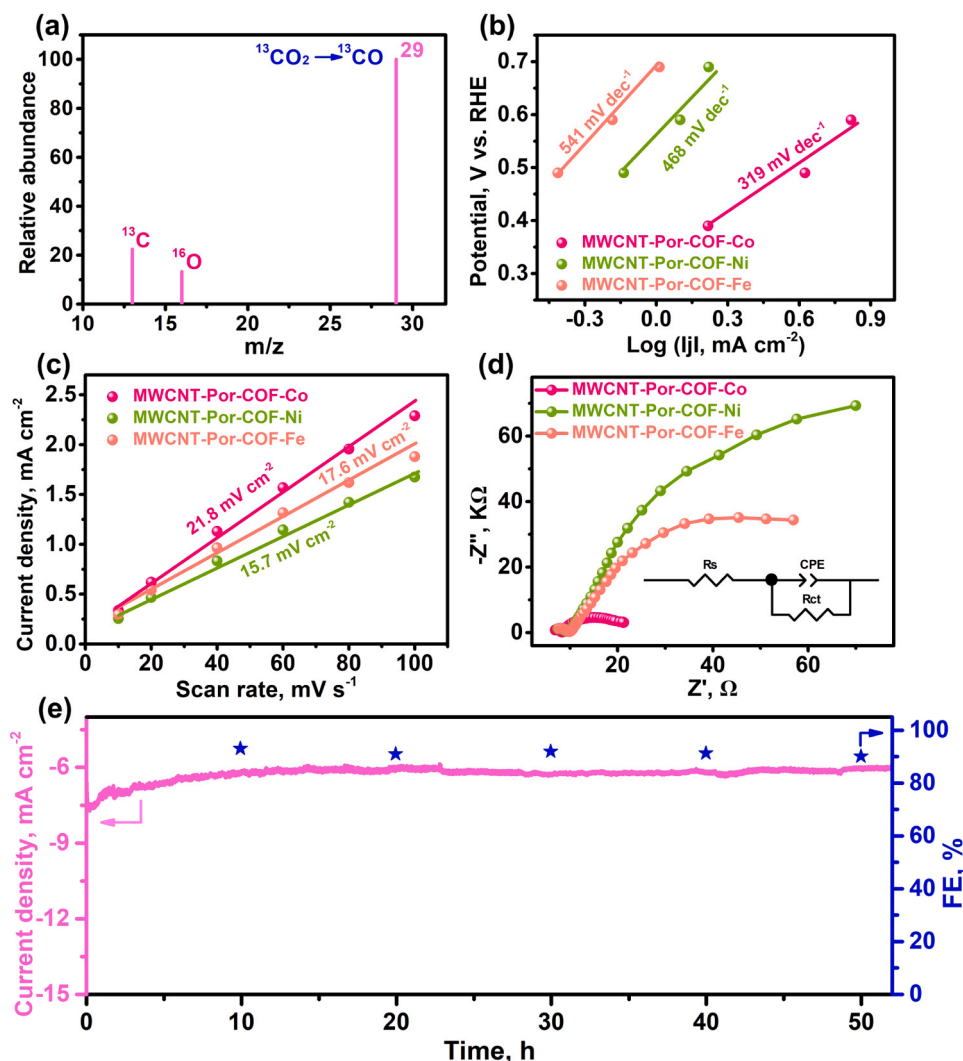
In order to better understand the  $\text{CO}_2\text{RR}$  kinetics, electrochemical impedance spectroscopy (EIS) measurements were tested. As shown in Fig. 3d, MWCNT-Por-COF-Co displays much smaller charge transfer resistance ( $10.1 \Omega$ ) compared to MWCNT-Por-COF-Ni ( $208.5 \Omega$ ) and MWCNT-Por-COF-Fe ( $71.9 \Omega$ ). This demonstrates a faster charge transfer kinetics exist in the MWCNT-Por-COF-Co, which is favorable for the electrocatalytic  $\text{CO}_2\text{RR}$  performance. Furthermore,  $\text{CO}_2$  adsorption isotherms of MWCNT-Por-COF-M were measured (Fig. S31). The results show that the adsorption capacity of MWCNT-Por-COF-Co ( $8.86 \text{ cm}^3 \text{ g}^{-1}$ ) is higher than that of MWCNT-Por-COF-Ni ( $7.37 \text{ cm}^3 \text{ g}^{-1}$ ) and MWCNT-Por-COF-Fe ( $4.61 \text{ cm}^3 \text{ g}^{-1}$ ) (298 K), demonstrating that different metal centers show different  $\text{CO}_2$  adsorption capacity, in

accordance with above experiment results. The long-term  $\text{CO}_2\text{RR}$  stability of the MWCNT-Por-COF-Co was examined using current-time ( $i$ - $t$ ) method at  $-0.7 \text{ V}$  in  $0.5 \text{ M KHCO}_3$ . As shown in Fig. 3e, small current density fluctuations and  $\text{FE}_{\text{CO}}$  is detected up to 50 h (CO is analyzed by GC). Moreover, the corresponding  $\text{FE}_{\text{CO}}$  can be maintained at values of  $\sim 90\%$ , which indicates that MWCNT-Por-COF-Co possesses prominent stability during the  $\text{CO}_2\text{RR}$  process.

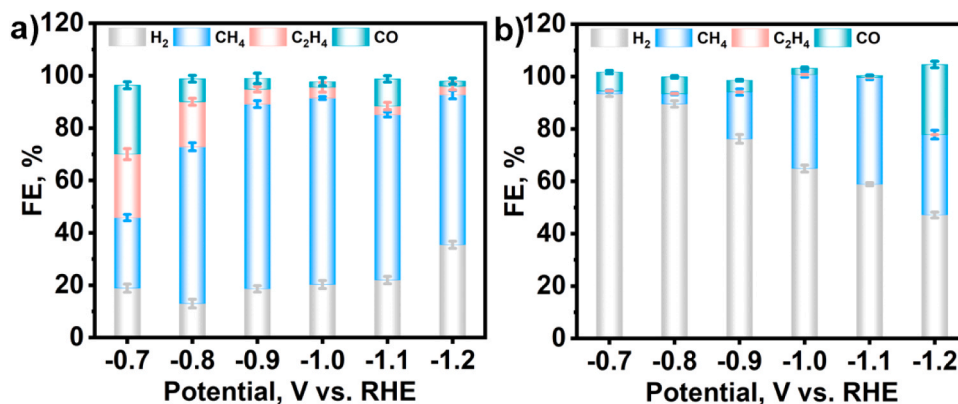
#### 3.4. Electrocatalytic $\text{CO}_2\text{RR}$ performances in flow cell

To further demonstrate the effect of different metal centers on  $\text{CO}_2$  reduction products, The MWCNT-Por-COF-Cu was determined for  $\text{CO}_2\text{RR}$  activity. The electrocatalytic  $\text{CO}_2\text{RR}$  performances for MWCNT-Por-COF-Cu were firstly evaluated in  $\text{CO}_2$ -saturated  $0.5 \text{ M KHCO}_3$  aqueous solution through H-type electrochemical cell, and the results show only hydrogen is produced and nothing else was detected. However, when changed to three-compartment flow cell with MWCNT-Por-COF-Cu modified carbon paper electrode as the working electrode and  $1.0 \text{ M KOH}$  as electrolyte,  $\text{CH}_4$ ,  $\text{C}_2\text{H}_4$  and CO products were detected in reaction system at a wide potential from  $-0.7 \text{ V}$  to  $-1.2 \text{ V}$  vs. RHE. For MWCNT-Por-COF-Cu,  $\text{CH}_4$  is regarded as the dominant product with the highest  $\text{FE}_{\text{CH}_4}$  of  $71.2\%$  at  $-1.0 \text{ V}$ , along with  $4.1\%$   $\text{FE}_{\text{C}_2\text{H}_4}$  and  $2.1\%$   $\text{FE}_{\text{CO}}$  (Figs. 4a–4b and S32). In comparison with MWCNT-Por-COF-Cu, Por-COF-Cu merely displayed weak  $\text{CO}_2\text{RR}$  activity with the  $\text{FE}_{\text{CH}_4}$  of  $40.8\%$  at  $-1.1 \text{ V}$  and  $59.0\%$   $\text{FE}_{\text{H}_2}$ . Furthermore, the electrocatalytic  $\text{CO}_2$  conversion to  $\text{CH}_4$  activity of MWCNT-Por-COF-Cu is comparable to that some reported Cu-based catalysts (Table S2) [55–60]. The long-time durability tests of MWCNT-Por-COF-Cu was assessed at  $-1.0 \text{ V}$  in  $1.0 \text{ M KOH}$  (Fig. S33), the corresponding  $\text{FE}_{\text{CH}_4}$  can be retained at values  $\sim 70\%$  in 1 h test, which proved the stability of MWCNT-Por-COF-Cu during the  $\text{CO}_2\text{RR}$  process. Besides, to verify the carbon source of  $\text{CO}_2\text{RR}$  products, the isotopic experiment was performed by using  $^{13}\text{CO}_2$  as carbon source and the products were analyzed by gas chromatography and mass spectra. A peak at  $m/z = 17$  from  $^{13}\text{CH}_4$  (Fig. S34) could be observed in MS spectrum, indicating the carbon sources of  $\text{CH}_4$





**Fig. 3.** (a) The GC-MS test of MWCNT-Por-COF-Co of  $^{13}\text{CO}$  recorded under  $^{13}\text{CO}_2$  atmosphere. (b) Tafel slopes, (c) Cdl, and (d) EIS curves for MWCNT-Por-COF-M (M: Co, Ni, Fe). (e) Long-term stability test of MWCNT-Por-COF-Co at  $-0.7$  V.



**Fig. 4.** Electrocatalytic performance of MWCNT-Por-COF-Cu (a) and Por-COF-Cu (b) at different applied potentials ( $-0.7$  to  $-1.2$  V).

indeed derive from the  $\text{CO}_2$ .

### 3.5. Mechanism analysis

Based on the above analysis and previously reported works [36,39], a feasible mechanism was proposed for MWCNT-Por-COF-M (Co, Ni, Fe)

(Fig. S35). In the electrocatalytic  $\text{CO}_2$ -to- $\text{CO}$  process, CNT acts as conductive platform improving the electron transfer in the material. Thanks to the covalent connection between CNT and Pro-COF-M (Co, Ni, Fe) as well as the vertical integration mode of them, electrons in CNT could continuously transfer to porphyrin plane of Pro-COF-M (Co, Ni, Fe) via connected covalent bonds. For the electronic character of

porphyrin and conjugated structure in Pro-COF-M (Co, Ni, Fe) layer, the electrons could be fluently transmitted to metal active sites for CO<sub>2</sub> reduction. This combination mode is superior to that without covalent for the dispersion of Pro-COF-M (Co, Ni, Fe) and electrons transfer between interfaces and within Pro-COF-M (Co, Ni, Fe) component, thus leading to largely enhanced electrocatalytic CO<sub>2</sub>RR performance.

As for the MWCNT-Por-COF-Cu, in order to further clarify the mechanism of MWCNT-Por-COF-Cu in electrocatalytic CO<sub>2</sub>-to-CH<sub>4</sub>, the XRD, XPS, Auger spectrum, SEM, TEM and HR-TEM of MWCNT-Por-COF-Cu after electrocatalytic CO<sub>2</sub>RR were tested. The PXRD patterns, SEM morphology and XPS spectra of MWCNT-Por-COF-Cu are no obvious change before and after electrocatalytic CO<sub>2</sub>RR (Fig. S36-S37, S38a-b). However, ultra-small particles (ca. 2 nm) with the lattice fringe of 0.21 nm could be observed in the high-resolution TEM image (Fig. S38c-d) [61], corresponding to the (111) plane of Cu<sup>0</sup>. The Cu LMM Auger spectra (Fig. S39) after CO<sub>2</sub>RR shows a peak centered at 567.8 eV corresponding to the Cu<sup>0</sup>, while the Cu<sup>+</sup> peak was not obvious. The results of HRTEM and Auger spectrum indicate that Cu<sup>0</sup> species (metallic Cu nanoclusters) may be generated during electrocatalytic CO<sub>2</sub>RR test. The Cu ions in MWCNT-Por-COF-Cu were converted in-situ into Copper-based nanoclusters, which act as real active sites for electrocatalytic CO<sub>2</sub>-to-CH<sub>4</sub> process, and this mechanism is similar to the reported literatures [58,62]. This restructuring behavior of MWCNT-Por-COF-Cu leads to different catalytic products.

#### 4. Conclusions

In summary, we have explored a new model of covalent connection MWCNT-Por-COF-M for efficient electrocatalytic CO<sub>2</sub>-to-CO conversion. This integration could tightly combine Por-COF and CNT together with uniform distribution and controlled electronic transfer pathway in electrocatalytic process. The experiments results showed that MWCNT-Por-COF-M (M: Co, Ni, Fe) composites show higher electrocatalytic activity and Faraday efficiency compared to the pure Por-COF-M. In particular, the MWCNT-Por-COF-Co shows the highest FE<sub>CO</sub> up to 99.3% at -0.6 V, along with a current density of 18.77 mA cm<sup>-2</sup> and TOF of 70.6 s<sup>-1</sup> at -1.0 V. It is clarified that the superior electrocatalytic activity of MWCNT-Por-COF-Co is mainly attributed to more efficient electron transfer for the effective integration mode of components. Besides, we also discussed the electrocatalytic CO<sub>2</sub> reduction activity of MWCNT-Por-COF-Cu in 1.0 M KOH by flow cell. The results show that MWCNT-Por-COF-Cu exhibits the highest CH<sub>4</sub> faradaic efficiency of 71.2% compared to the MWCNT-Por-COF. The results of HRTEM and Auger spectrum revealed that the high performance of MWCNT-Por-COF-Cu could be attributed to the generated Copper-based nanoclusters during the electrocatalytic CO<sub>2</sub>RR process. This work provides a new strategy for further wise constructing COF-based composites for efficient electrocatalytic CO<sub>2</sub>RR.

#### CCRediT authorship contribution statement

**Hong Dong:** Conceptualization, Investigation, Writing – review & editing. **Meng Lu:** Writing – review & editing. **Ya Wang:** Formal analysis. **Hong-Liang Tang:** Data curation. **Di Wu:** Data curation. **XiaoJun Sun:** Project administration. **Feng-Ming Zhang:** Supervision, Project administration.

#### Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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#### Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at doi:10.1016/j.apcatb.2021.120897.

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